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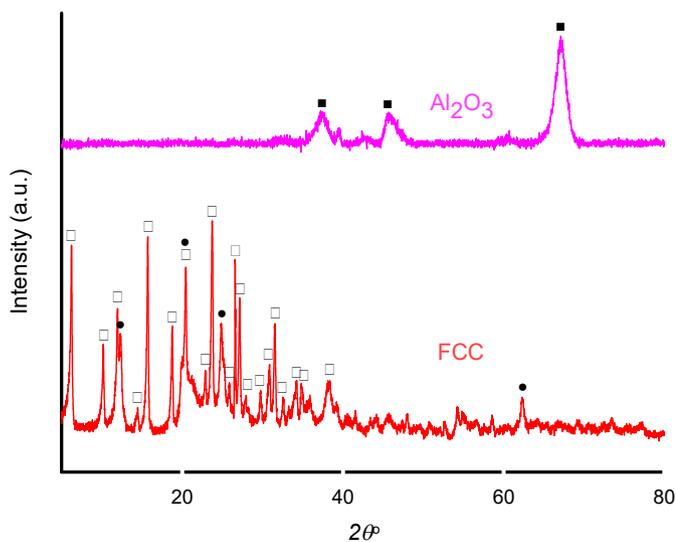
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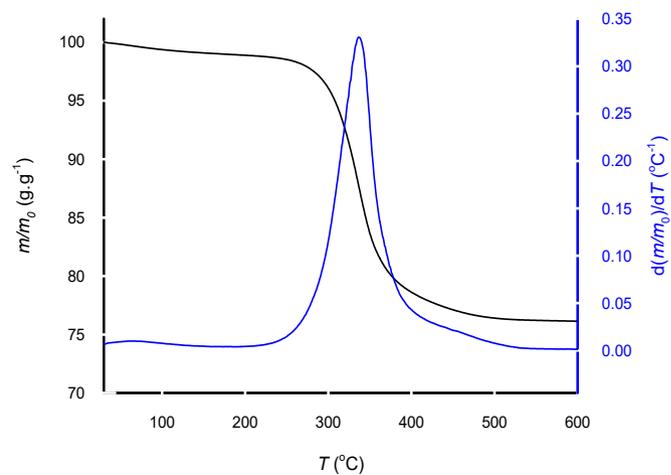
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**FIGURE A1** X-ray powder diffraction over fresh  $\gamma$ - $\text{Al}_2\text{O}_3$  and FCC: squares -  $\gamma$ - $\text{Al}_2\text{O}_3$ ; triangles - Zeolite Y; circles - Kaolinite; rhombus -  $\text{SiO}_2$ .

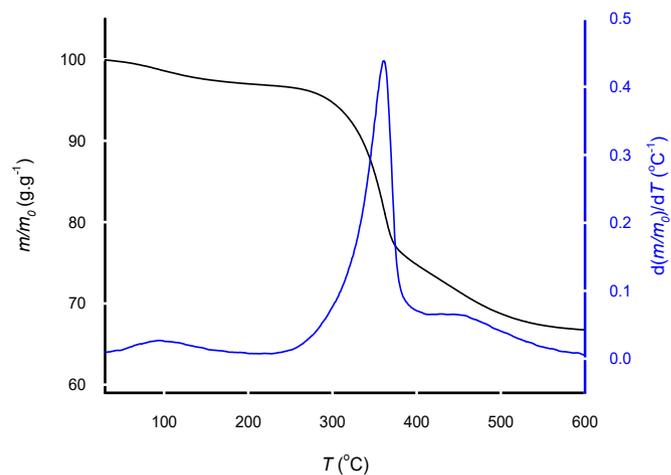


**FIGURE A2** TGA (black curve) and DTG (blue curve) analysis of  $\text{Al}_2\text{O}_3$  bed residue in air (60 mL/min).



## APPENDIX

### A SUPPLEMENTARY INFORMATION

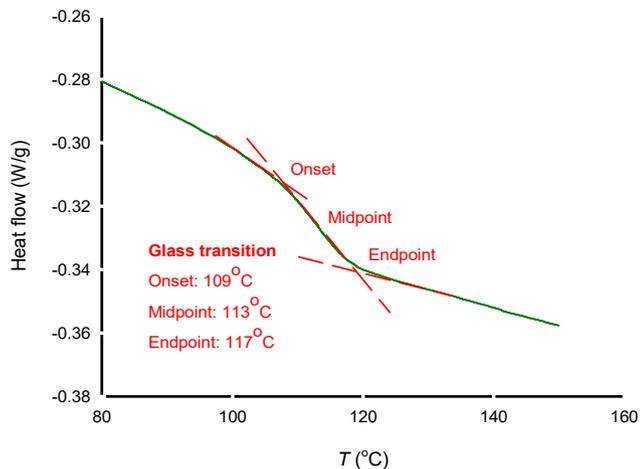


**FIGURE A3** TGA (black curve) and DTG (blue curve) analysis of FCC bed residue in air (60 mL/min).

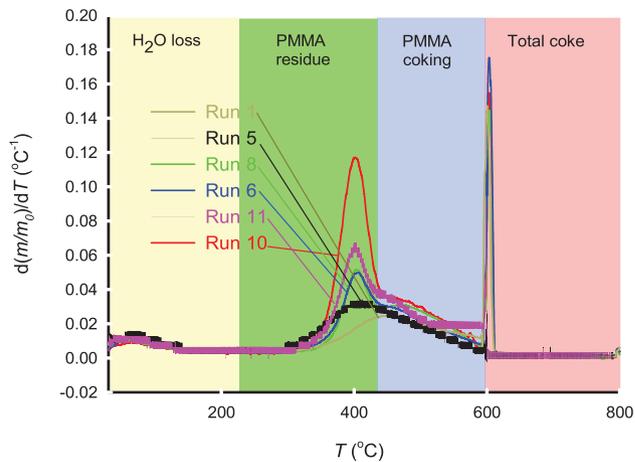
**TABLE A1** PMMA depolymerization carbon balance.

Catalyst	$T$ °C	$U_g$ mm s <sup>-1</sup>	$m$ g	$X_{PMMA}$ * %	$Y_{MMA}$ %	$Y_{acet}$ %	$S_{MMA}$ %	$S_{acet}$ %	$C_{resid}$ ** % mass	CO % mass	CH <sub>4</sub> % mass	CO <sub>2</sub> % mass	$C_{recov}$ % mass
Al <sub>2</sub> O <sub>3</sub>	380	38	10	42.60	13.90	0.29	32.62	0.68	58.95	1.42	2.48	1.93	78.97
FCC	380	38	10	94.52	1.65	1.16	1.75	1.22	59.35	6.82	1.28	4.82	75.07
FCC	350	38	7	63.99	1.50	1.38	2.34	2.15	69.46	5.55	0.73	2.41	81.03
FCC	350	50	7	74.62	1.20	0.59	1.61	0.79	72.06	3.30	0.74	4.01	81.91
Al <sub>2</sub> O <sub>3</sub>	380	50	7	65.03	46.00	0.24	70.73	0.38	43.87	0.08	0.85	11.40	102.45
Al <sub>2</sub> O <sub>3</sub>	350	50	10	23.33	3.86	0.39	16.54	1.69	83.51	2.17	2.12	1.31	93.36
FCC	380	38	7	87.66	2.78	1.32	3.17	1.51	57.37	8.34	1.36	5.50	76.67
Al <sub>2</sub> O <sub>3</sub>	350	38	10	32.97	4.79	0.52	14.53	1.56	64.58	1.62	1.73	1.57	74.80
FCC	380	50	10	84.65	1.35	0.67	1.60	0.79	61.28	4.52	1.43	9.78	79.02
Al <sub>2</sub> O <sub>3</sub>	350	38	7	21.89	19.72	2.61	90.07	11.93	69.41	2.43	1.36	1.11	96.64
Al <sub>2</sub> O <sub>3</sub>	350	50	7	42.82	26.45	0.99	61.77	2.30	66.12	1.64	1.22	6.49	102.92
FCC	350	50	10	73.95	1.14	4.05	1.54	5.48	71.58	6.51	0.86	2.97	87.10

\* TGA, \*\*LECO



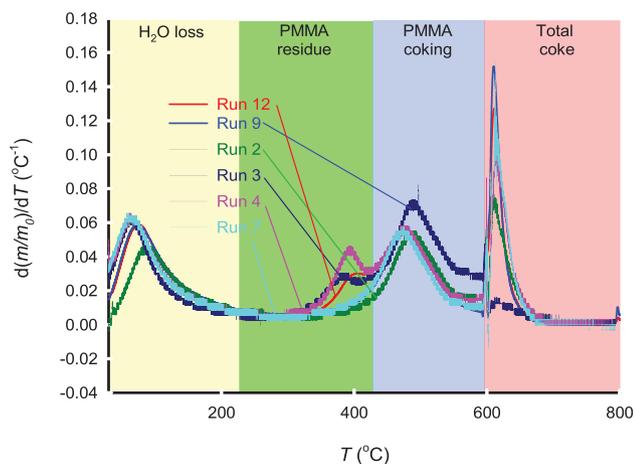
**FIGURE A4** DSC analysis of pure PMMA gives onset  $T_g = 109$  °C; midpoint = 113 °C; endpoint = 117 °C.



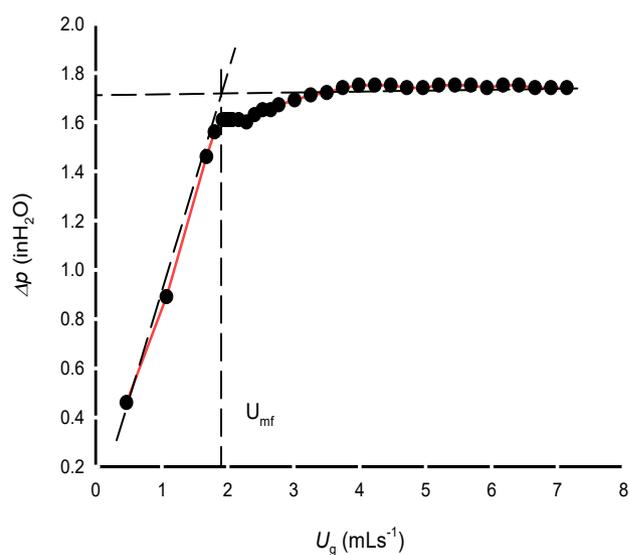
**FIGURE A5** DTG profile from the decomposition of solid residue for  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> bed.

**TABLE A2** Average molecular weight and free volume change with each recycling cycle.

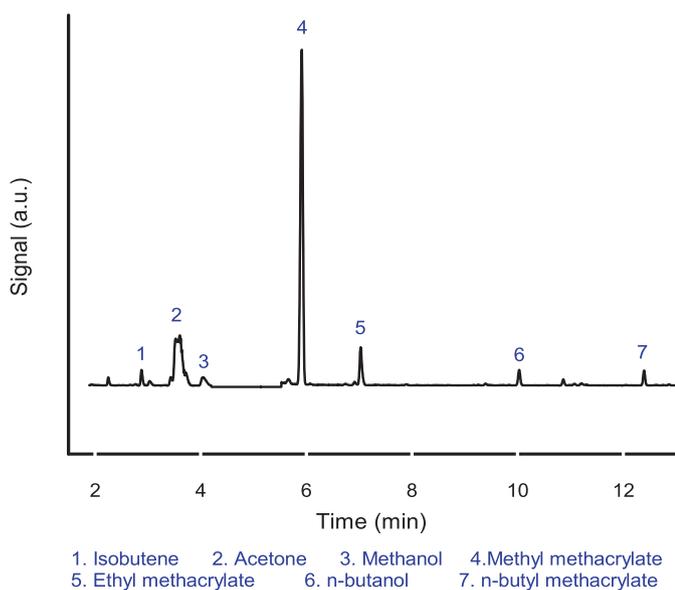
Cycle	$M_w$ g mol <sup>-1</sup>	$M_n$ g mol <sup>-1</sup>	DP	$v_f$ mL g <sup>-1</sup>	$v$ mL g <sup>-1</sup>
0	120100	77300	773	$2.43 \times 10^{-3}$	$960 \times 10^{-3}$
1	115400	76300	763	$8.71 \times 10^{-3}$	$915 \times 10^{-3}$
3	112000	73400	734	$14.11 \times 10^{-3}$	$892 \times 10^{-3}$
5	110600	70900	709	$36.62 \times 10^{-3}$	$896 \times 10^{-3}$



**FIGURE A6** DTG profile from the decomposition of solid residue for FCC bed.



**FIGURE A8** Determining  $U_{mf}$  of SiC bed by pressure drop method: the pressure drop between the inlet and outlet of the reactor is measured with different carrier gas velocities.<sup>[32]</sup>  $U_{mf}$  is determined by the junction between the linear regression line from the pack-bed region (the rising part) and the bubbling fluidization region (the region with constant  $\Delta p$ ).<sup>[33]</sup>



**FIGURE A7** GC-MS chromatogram of liquid fraction in full scan mode.